

# Coal Transformation: Clean Coal

Dr. Steve Son

Multiphase Combustion  
Laboratory

Mechanical Engineering

Purdue University

March 1, 2007



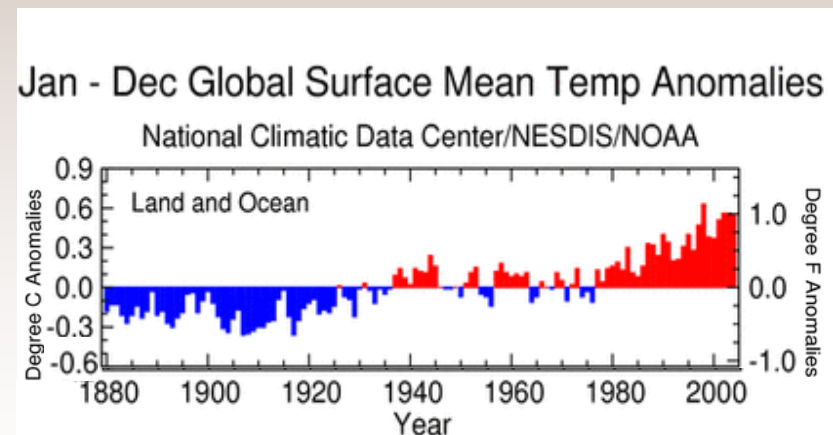
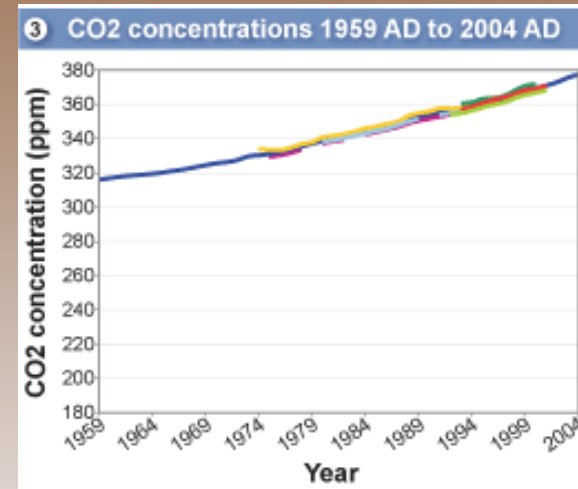
Wade Utility Plant, Purdue University

# Overview

- Background
  - Environmental Concerns
  - Legislation
- Proposed Solutions & Motivation
  - IGCC
  - Oxy-Fuel
  - Scrubbing
  - Economics estimates
- What is Oxy-Fuel?
  - Background
  - Previous studies
  - Technical issues
- Purdue Combustion Studies Beginning
  - Constant volume or pressure Combustion
  - Pressurized Systems
  - Future areas?
    - Chemical Looping
    - Aluminum combustion with CO<sub>2</sub>

# Background

- Environmental Concerns
  - “Greenhouse Effect” has led to 1°F average increase over 20 years
  - Current rate is 0.32°F per decade
  - NO<sub>x</sub> contributes to Acid Rain and “greenhouse effect”



Source: [www.epa.gov](http://www.epa.gov)

# Background

- Legislation
  - President's Clear Skies Initiative
    - Reduce NO<sub>x</sub> 67% from 2000 levels and SO<sub>2</sub> 73% from 2000 levels by 2018
  - Greenhouse Gas (GHG) Intensity
    - Reduce intensity (tons gas/ \$M GDP) 18% by 2012
  - International Kyoto Protocol
    - UN rule to reduce GHG emissions 5% by 2012
    - Binding to countries who ratified (>55% of world emissions)

# Proposed Solutions

- Longer Term

- Nuclear

- Alternative Energy

- Renewable

- Wind, Solar, Biofuels



- Coal will be used in foreseeable future

- **Coal is the most abundant domestic fuel and it remains the lowest cost fuel for power generation**

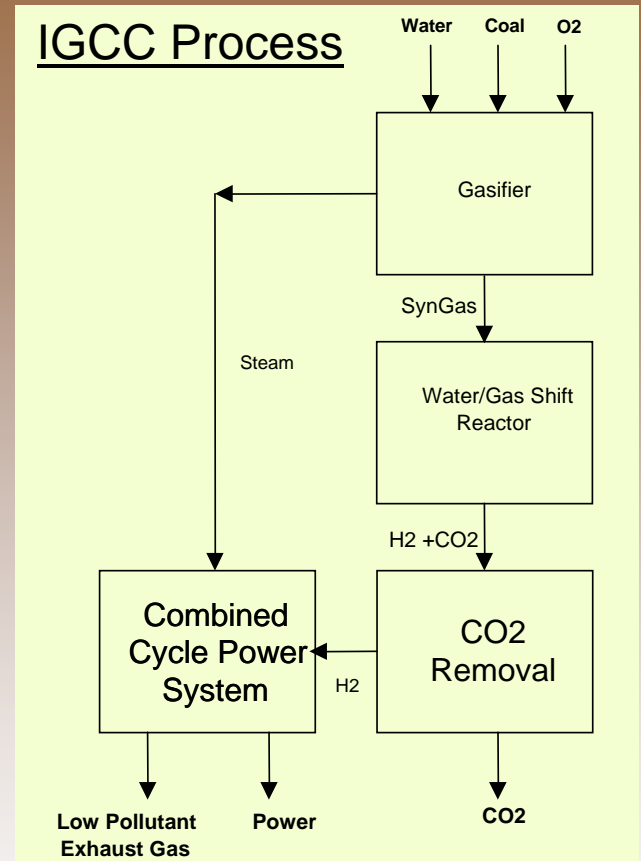
- Increase Efficiency

- Ultra Super-Critical Pulverized Coal

- Integrated Gasification Combined Cycle (IGCC)

- Higher Efficiency

- Produces usable hydrogen



# Nearer Term Options for Clean Coal

- Three approaches are presently seen as the front runners:
  - **Oxygen combustion**
    - Concentrates CO<sub>2</sub>
    - Reduces NO<sub>x</sub>
  - **Amine (or others) scrubbing** for new or existing plants
    - Extracts the CO<sub>2</sub> from the flue gas using a regenerable sorbent-catalyst such as monoethanolamine (or MEA)
  - **IGCC**
    - Concentrates CO<sub>2</sub>
    - Produces multi-use syngas
  - *“Some current studies show oxygen combustion as the least costly while others lean toward IGCC, indicating that the jury is still out.”* (Williams et al., BR-1779, 2006)

# Economics of Clean Coal

- Many uncertainties still exist when comparing costs of new technologies
  - Scales
  - Availability of Technology
  - Repair costs
  - Lost Energy Costs
  - Disposal/salvage Costs
- However, taking published studies on cost data and comparing to real world numbers, the following calculations result:

	<b>Capital Costs</b>	<b>Annual Cost</b>	<b>Total cost (400 MW)</b>
<b>Method</b>	<b>(\$/MW)</b>	<b>(\$/ {year * MW})</b>	<b>(\$ for year 1)</b>
Amine	\$899,297	\$257,496	\$462,717,326.84
Oxyfuel	\$966,663	\$220,878	\$475,016,480.26
IGCC	\$1,483,840	\$192,750	\$670,636,013.14

**Notes:**

- 1) All numbers in \$US 2006
- 2) Amine & Oxyfuel are retrofit costs, IGCC is new plant
- 3) 20 years is the assumed life of retrofitted plant

**References:**

- Smith LA, Gupta N, Sass BM, Bubenik T, Byer C, Bergman P. "Engineering and economic assessment of carbon dioxide sequestration in saline formations." Journal of Energy and Environmental Research 2002; 2:5–22.
- Singh D, Croiset E, Douglas PL, Douglas MA. "Techno-economic study of CO2 capture from an existing coal-fired power plant: MEA scrubbing Vs. O2/CO2 recycle combustion." Energy Conversion Management 2003;44:3073–91.

# Economics of Clean Coal

- What does this mean to Indiana?
  - Costs of revamping “The Big 10” estimated
  - 50 years assumed as life of plant
  - Retrofits include boiler and turbine refurbishment at 50 years from original boiler install



# Economics of Clean Coal

## Without fuel costs

	<i>Design Output (MW)</i>	<i>Amine Retrofit Cost</i>	<i>Oxyfuel Retrofit Cost</i>	<i>IGCC Replacement Cost</i>
Gibson	3340	\$16,520,853,638	\$10,630,647,234	\$15,811,025,710
Tanner's Creek	1099	\$5,436,053,338	\$3,497,928,536	\$5,202,490,196
Rockport	1300	\$6,430,272,374	\$4,137,677,067	\$6,153,992,043
Schahfer	2200	\$10,881,999,402	\$7,002,222,729	\$10,414,448,072
Petersburg	1880	\$9,299,163,125	\$5,983,717,605	\$8,899,619,262
Clifty Creek	1300	\$6,430,272,374	\$4,137,677,067	\$6,153,992,043
Cayuga	1193	\$5,901,011,494	\$3,797,114,416	\$5,647,471,159
Merom	1080	\$5,342,072,434	\$3,437,454,794	\$5,112,547,235
Stout/Harding St.	1185	\$5,861,440,587	\$3,771,651,788	\$5,609,600,439
Wabash River	668	\$3,304,170,728	\$2,126,129,447	\$3,162,205,142

## With fuel costs

	<i>Design Output (MW)</i>	<i>Amine Retrofit Cost</i>	<i>Oxyfuel Retrofit Cost</i>	<i>IGCC Replacement Cost</i>
Gibson	3340	\$47,729,813,638	\$41,839,607,234	\$37,145,275,710
Tanner's Creek	1099	\$15,705,109,338	\$13,766,984,536	\$12,222,352,696
Rockport	1300	\$18,577,472,374	\$16,284,877,067	\$14,457,742,043
Schahfer	2200	\$31,438,799,402	\$27,559,022,729	\$24,466,948,072
Petersburg	1880	\$26,865,883,125	\$23,550,437,605	\$20,908,119,262
Clifty Creek	1300	\$18,577,472,374	\$16,284,877,067	\$14,457,742,043
Cayuga	1193	\$17,048,403,494	\$14,944,506,416	\$13,267,758,659
Merom	1080	\$15,433,592,434	\$13,528,974,794	\$12,011,047,235
Stout/Harding St.	1185	\$16,934,080,587	\$14,844,291,788	\$13,178,787,939
Wabash River	668	\$9,545,962,728	\$8,367,921,447	\$7,429,055,142

# Economics of Clean Coal

- What if 50 years isn't realistic?
  - Assume Boiler and turbine retrofits are not necessary

	<i>Design Output (MW)</i>	<i>Amine Retrofit Cost</i>	<i>Oxyfuel Retrofit Cost</i>	<i>IGCC Replacement Cost</i>
Gibson	3340	\$15,904,217,953	\$14,294,657,503	\$14,612,800,710
Tanner's Creek	1099	\$5,233,154,350	\$4,703,541,496	\$4,808,223,946
Rockport	1300	\$6,190,264,473	\$5,563,788,848	\$5,687,617,043
Schahfer	2200	\$10,475,832,185	\$9,415,642,666	\$9,625,198,072
Petersburg	1880	\$8,952,074,776	\$8,046,094,642	\$8,225,169,262
Clifty Creek	1300	\$6,190,264,473	\$5,563,788,848	\$5,687,617,043
Cayuga	1193	\$5,680,758,089	\$5,105,846,228	\$5,219,482,409
Merom	1080	\$5,142,681,254	\$4,622,224,582	\$4,725,097,235
Stout/Harding St.	1185	\$5,642,664,154	\$5,071,607,527	\$5,184,481,689
Wabash River	668	\$3,180,843,591	\$2,858,931,501	\$2,922,560,142

With fuel / 15 years

	<i>Design Output (MW)</i>	<i>Amine Retrofit Cost</i>	<i>Oxyfuel Retrofit Cost</i>	<i>IGCC Replacement Cost</i>
Gibson	3340	\$20,204,406,622	\$17,983,325,321	\$17,831,725,710
Tanner's Creek	1099	\$6,648,096,670	\$5,917,267,823	\$5,867,385,196
Rockport	1300	\$7,863,990,601	\$6,999,497,880	\$6,940,492,043
Schahfer	2200	\$13,308,291,787	\$11,845,304,104	\$11,745,448,072
Petersburg	1880	\$11,372,540,254	\$10,122,350,780	\$10,037,019,262
Clifty Creek	1300	\$7,863,990,601	\$6,999,497,880	\$6,940,492,043
Cayuga	1193	\$7,216,723,683	\$6,423,385,362	\$6,369,236,159
Merom	1080	\$6,533,161,423	\$5,814,967,469	\$5,765,947,235
Stout/Harding St.	1185	\$7,168,329,894	\$6,380,311,529	\$6,326,525,439
Wabash River	668	\$4,040,881,324	\$3,596,665,064	\$3,566,345,142

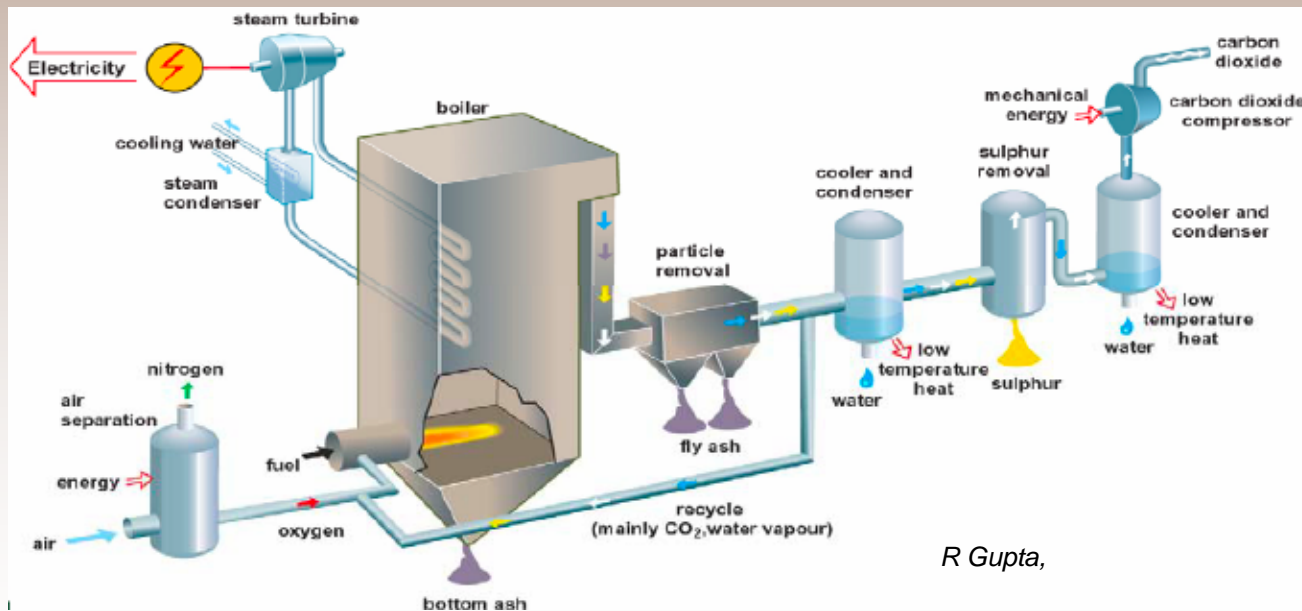
With fuel / 20 years

# Economics of Clean Coal

- If IGCC somewhat cheaper (for 50 years & many assumptions), why oxy-fuel?
  - Cost of retraining operators for IGCC not included
    - IGCC operation is more complex
  - Air separation units purchased for Oxy-fuel retrofit could be used later on IGCC replacements
    - Can lower future necessary capital funds
  - IGCC startup costs much larger
    - Oxy-fuel capital is 65% less
    - IGCC technology and experience improving, so oxy-fuel retrofit followed at some point by IGCC replacement may be better in some cases
  - If oxy-fuel boiler & turbine are upgraded to higher performance (efficiencies), less fuel would be used and the system would be more competitive with IGCC
    - For example, could utilize higher temperatures from oxygen combustion instead of using recycled flue gases to match original design

# What exactly is oxy-fuel?

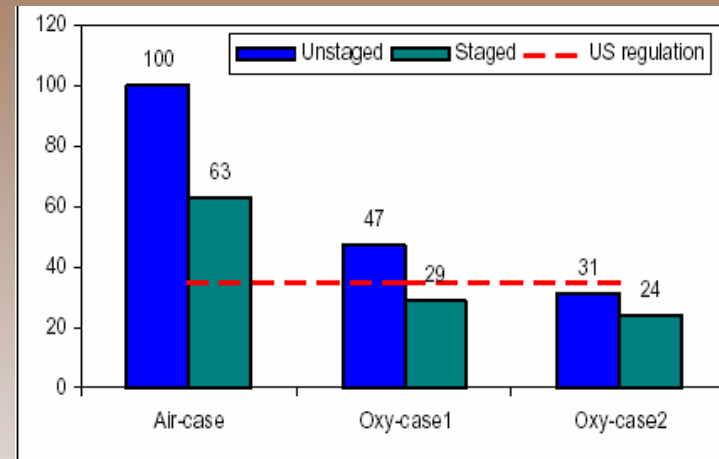
- Oxy-Fuel
  - Pure oxygen as oxidizer
  - Reduces or eliminates  $\text{NO}_x$
  - Increases  $\text{CO}_2$  concentration
    - Easier to recover
  - *Can be used in retrofit coal plants*



R Gupta,

# Previous Oxy-Fuel Studies

- Pollutants
  - NO<sub>x</sub> reduced
    - Can be further reduced
  - CO<sub>2</sub> concentrated >90%



(a) NO<sub>x</sub> emissions, normalised assuming the baseline value in air-case is 100. Dash line is US regulation 65 mg/MJ

*Oxy-fuel combustion in GHG Context – Status of Research, Technology and Assessment  
R Gupta, CRC for Coal in Sustainable Development  
Univ of Newcastle Australia  
Advanced Coal Workshop, Brigham Young University, Provo, Utah, 15-16th March 2005*

# Previous Oxy-Fuel Studies

- Flame and Heat Transfer
  - Instabilities observed
    - Can be overcome by increasing  $O_2$ , but increases cost
    - Can this be overcome by recycling hot exhaust (flue) gas (RFG)? Are optimized ignition and combustion possible?
  - Heat Transfer changed
    - No  $NO_x$ ,  $N_2$ , less CO to carry heat to boiler
      - Transport properties changed
    - Can likely be made to match air burning with RFG
    - Avoids changing plant electrical output

# Previous Oxy-Fuel Studies

- Retrofit
  - Most necessary technology is mature
    - Optimization should be only changes
  - Must find a place for CO<sub>2</sub>
    - No current large scale market
    - Must sequester and store
  - Can be adapted to future technological advances
    - IGCC using air separation unit from oxy-fuel retrofit
  - Pilot Studies already done
    - Companies such as Air Liquide and Alstom



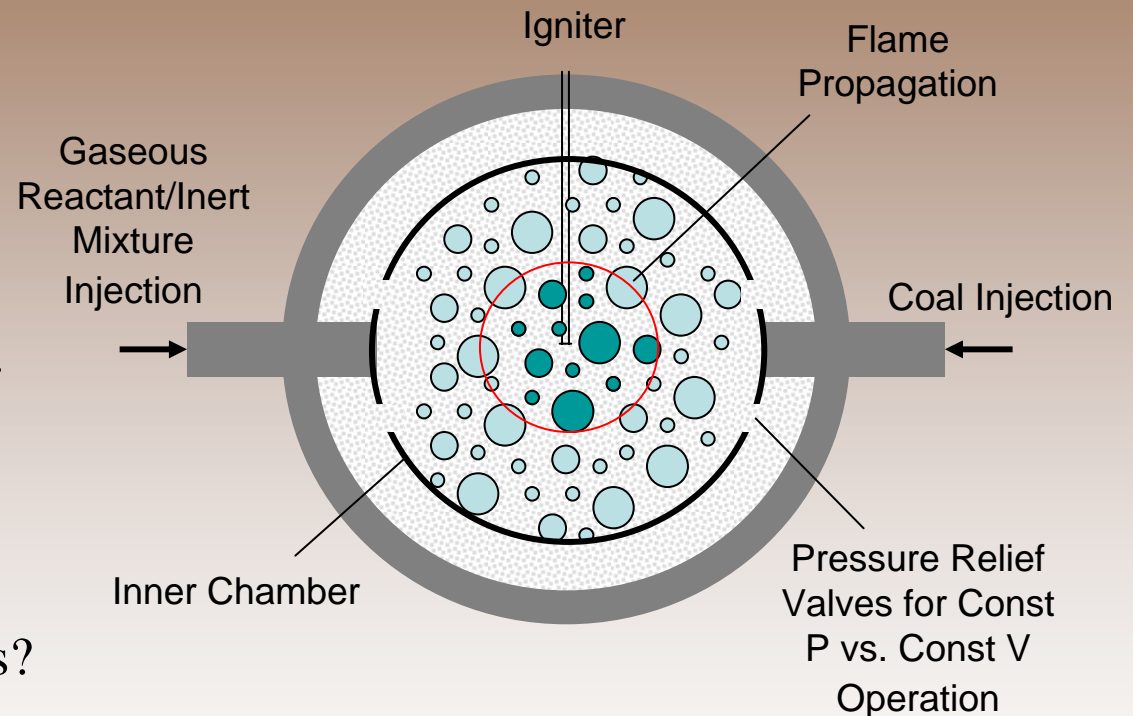
Jupiter Oxy-Fuel plant; Hammond, IN

*We are collaborating with Jupiter Oxygen Corporation, who is retrofitting 25 MW plant in Orville, Ohio; as well as developing an oxy-fuel pilot plant in Hammond, IN*

# Studies Beginning at Purdue

- Constant volume or pressure ignition and combustion
  - Flame and ignition characterization studies
  - Pollutant concentrations
  - RFG/O<sub>2</sub>% optimization
  - Comparisons with Jupiter pilot reactor
  - Indiana coals considered
- Pressurized studies
  - Control flame instabilities?
  - Future technology areas?
    - IGCC pressurized syngas
    - Chemical looping

## Funding from Indiana CCTR

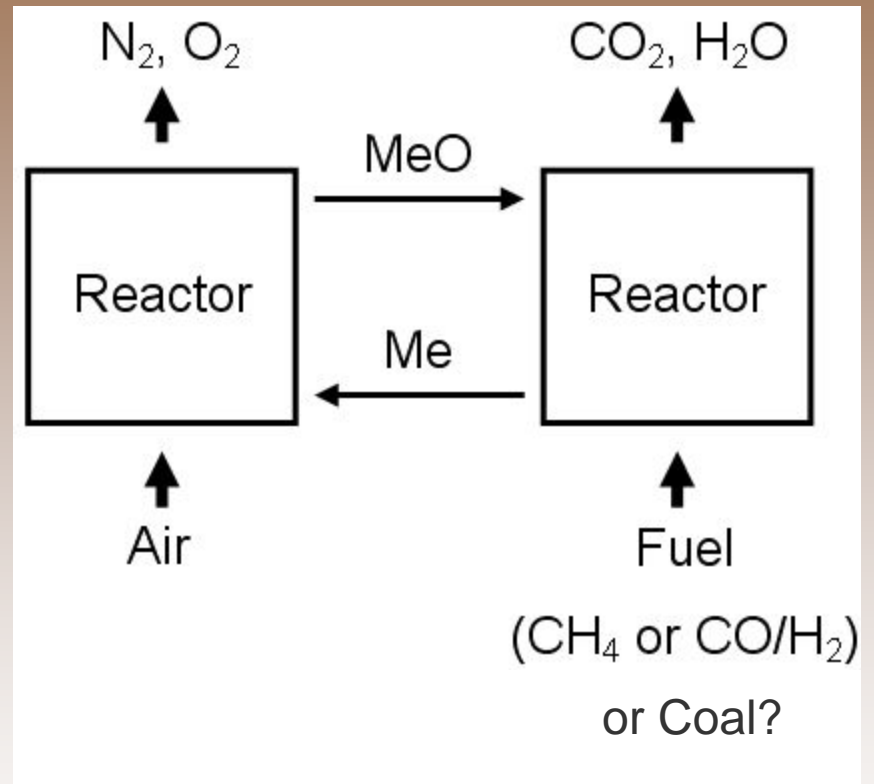


***Can hot RFG stabilize O<sub>2</sub>/CO<sub>2</sub>/Coal flame with lower O<sub>2</sub> concentration?***



# Some Future Areas

- Chemical Looping Combustion (CLC)
  - Uses metal oxides to provide oxygen for Oxy-Fuel
  - Potentially cheaper than cryogenic
  - Will pulverized coal work with CLC?
  - Survivability of cycled metal
- Can CO<sub>2</sub> be used as oxidizer instead of air?
  - For example, Al and Mg can burn with CO<sub>2</sub> as the oxidizer
  - Eliminates need for sequestration
  - Produces heat (could drive additional power generation) and CO that could be used to make alcohol fuel
  - Optimize for CO or C(s) products?



Note: MeO = Metal Oxide  
Me = Metal